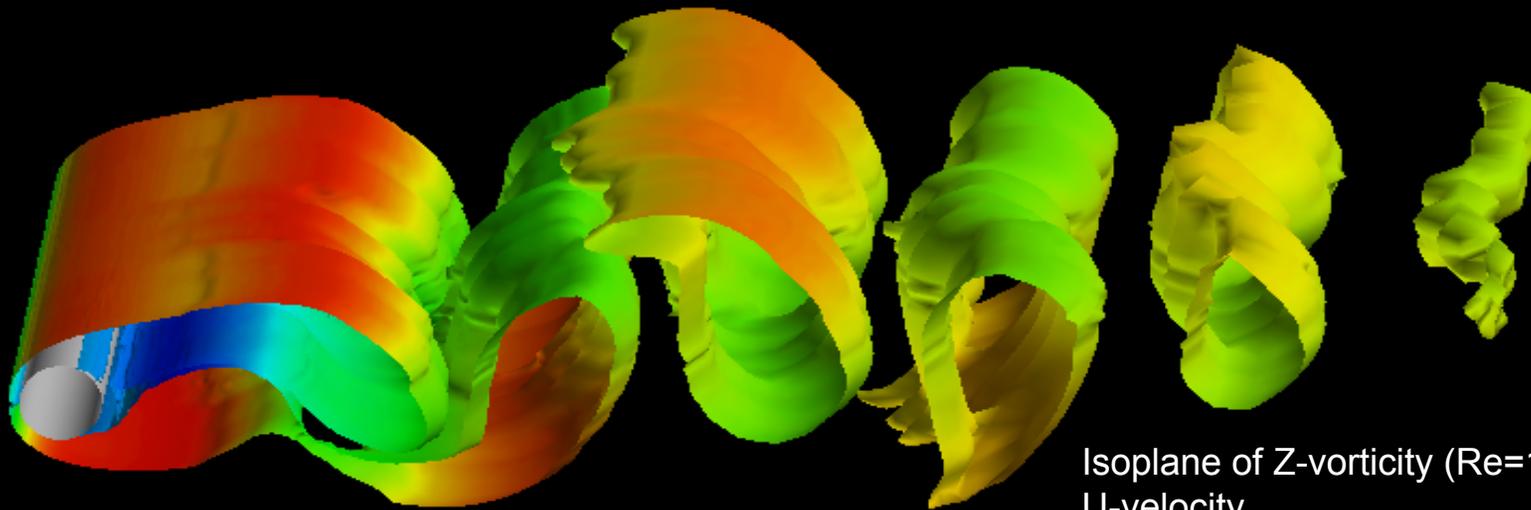
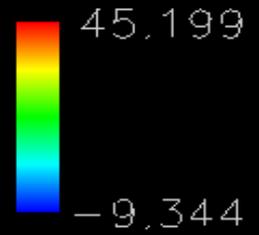


Vortex shedding in the cylinder wake



Isoplane of Z-vorticity ($Re=120$) coloured by U-velocity

Comparison between 2d and 3d results

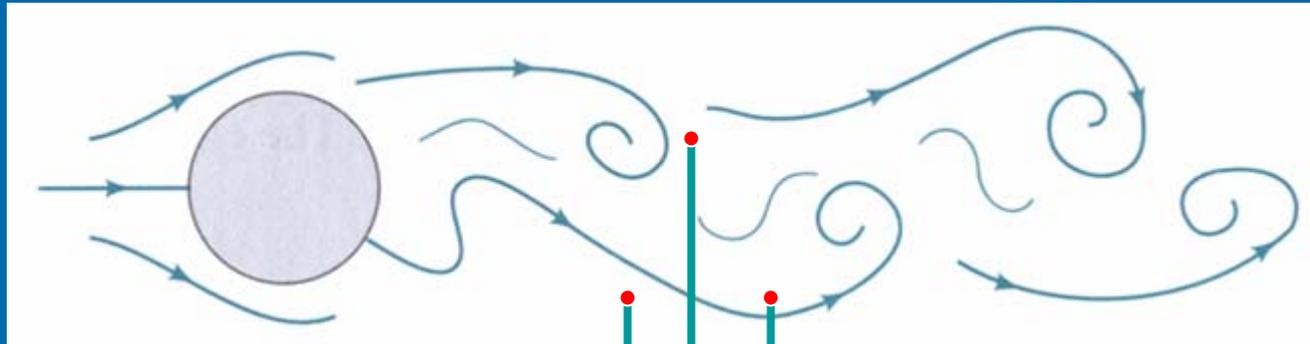
Acknowledgements



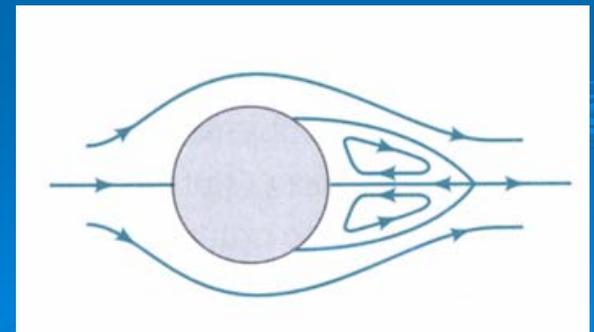
- @ Dr. Kelly Cohen
- @ Maj. Jim Forsythe
- @ Dr. Tom McLaughlin
- @ Maj. Scott Morton
- @ Dr. Stefan Siegel

Note the vortices ;-)

Introduction



The BIG question: will this setup work in three dimensions?



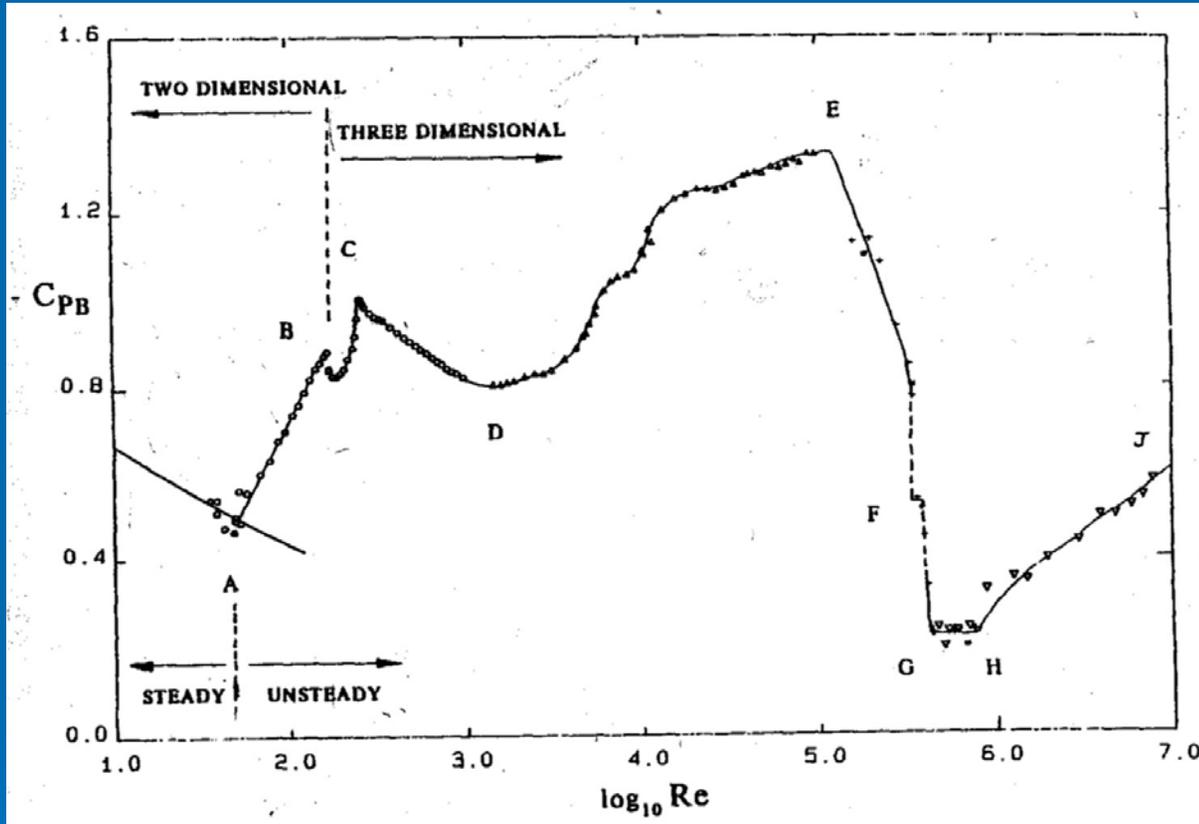
Sketches from: Munson, Young, Okiishi. *Fundamentals of Fluid Mechanics*. p 601.



- Background
- Motivation
- Research objective
- Literature survey
- CFD Computations (Results)
- POD analysis (Results)
- Suggestions / Recommendations

Background

Vortex shedding regimes



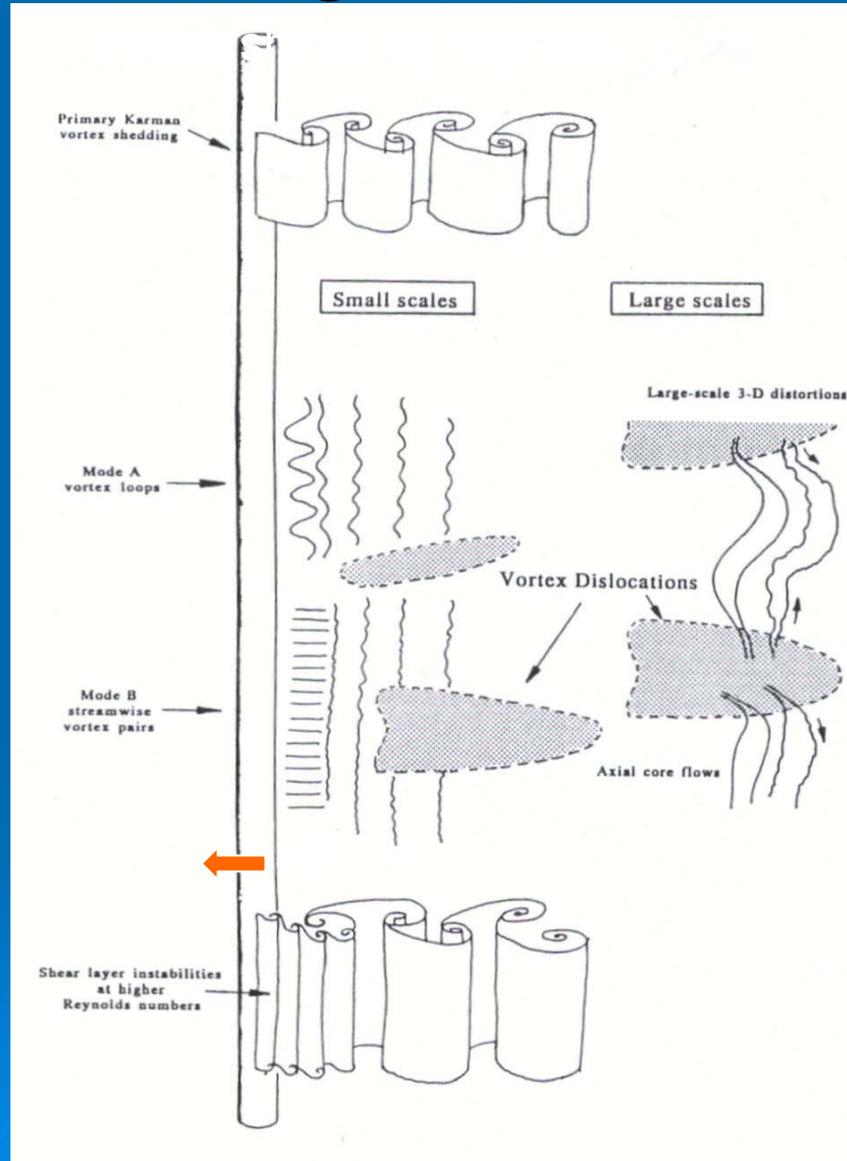
-A: laminar steady regime ($Re < 49$)

A-B: laminar vortex shedding ($49 < Re < 190$)

B-C: wake transition regime ($190 < Re < 260$)

C-D: fine scale regime ($260 < Re < 1000$)

Vortex shedding regimes (cont)



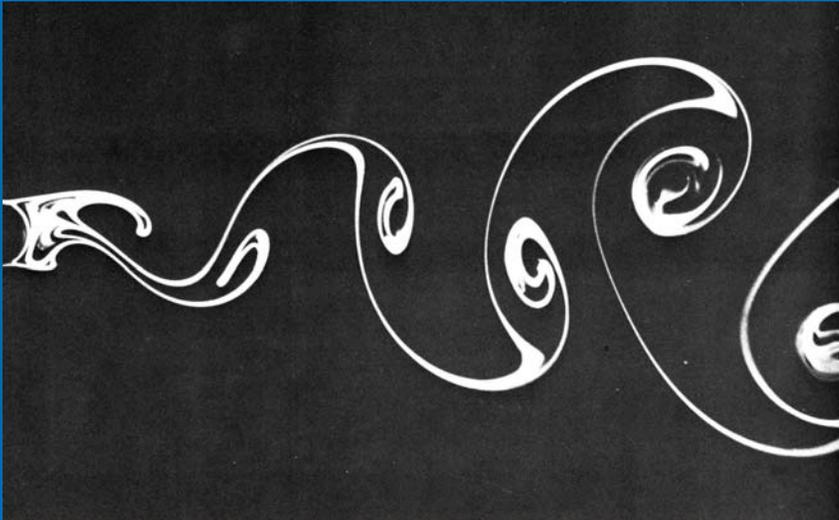
Background (cont)

Laminar vortex shedding ($Re=49-190$)



- Flow behaves (almost) 2 dimensional in spanwise direction, if care is taken to manipulate the boundary conditions

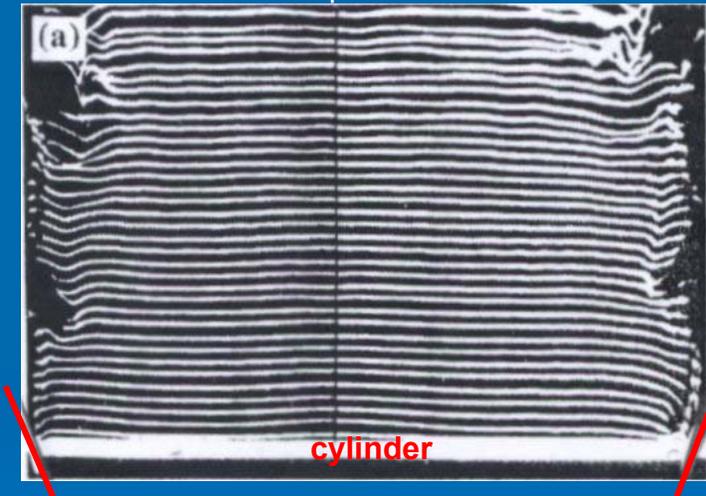
Side view



Von Karman vortex street; $Re=140$

Van Dyke, 1982

Top view



Parallel vortex shedding,
using angled endplates

Williamson, 1988

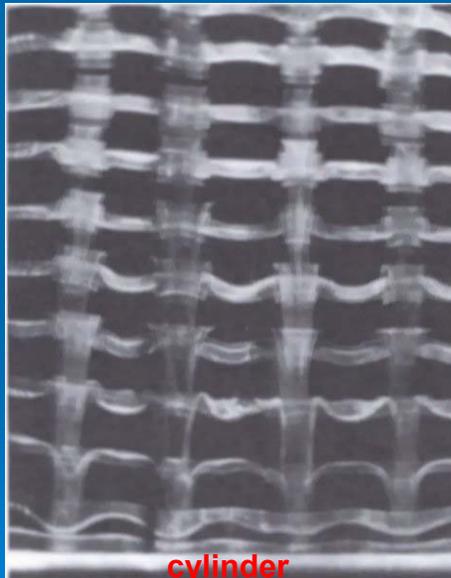
Background (cont)



Wake transition ($Re=190-260$)

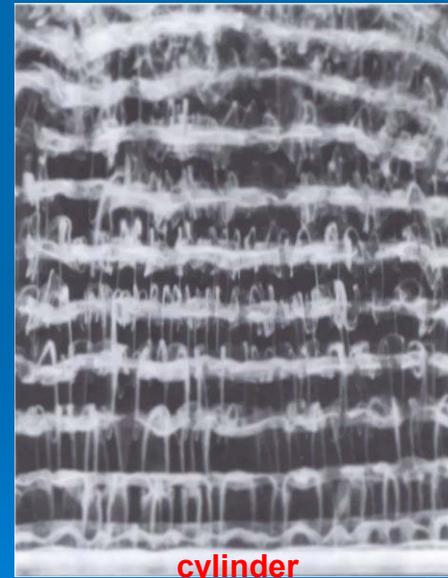
- Above $Re=190$ the wake becomes (really) 3 dimensional (the von Karman vortex street still persists)
- Large (mode A) and fine (mode B) scales due to shift in phase or frequency difference in spanwise direction

Top view



Mode A; $Re=180$
and above

Top view



Mode B; $Re=230$
and above



- Compare 3D with 2D cylinder simulations in order to see if the the control strategy to suppress the 2D flow, will also work in three dimensions.

Research objective



- The control strategy is based upon controlling the POD modes of the flow. So the main focus is on the comparison of the 2D and 3D POD modes.



- Wake flow of a cylinder at $Re=100$ and above exhibits self-excited oscillations, which are sustained by the flow itself → absolute instability
- The period of oscillations is determined by the St number, which is a continuous function of the Re number
(good check case for numerical results)

Sources: Gillies, 1995/97; Blevins, 1990; Williamson 1996

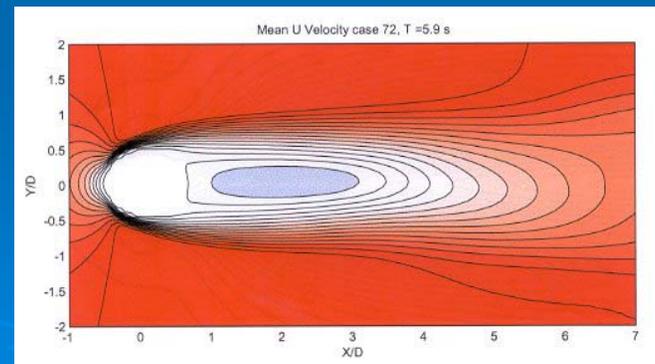
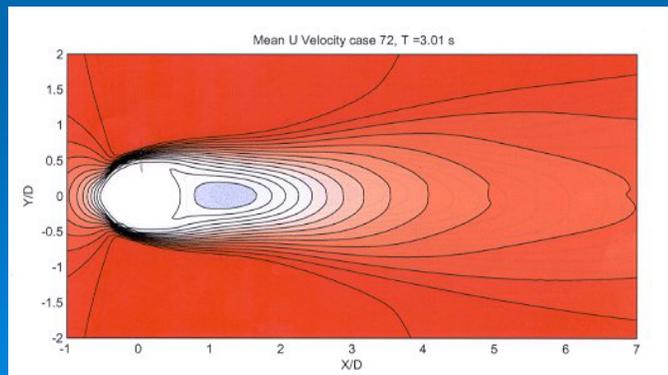
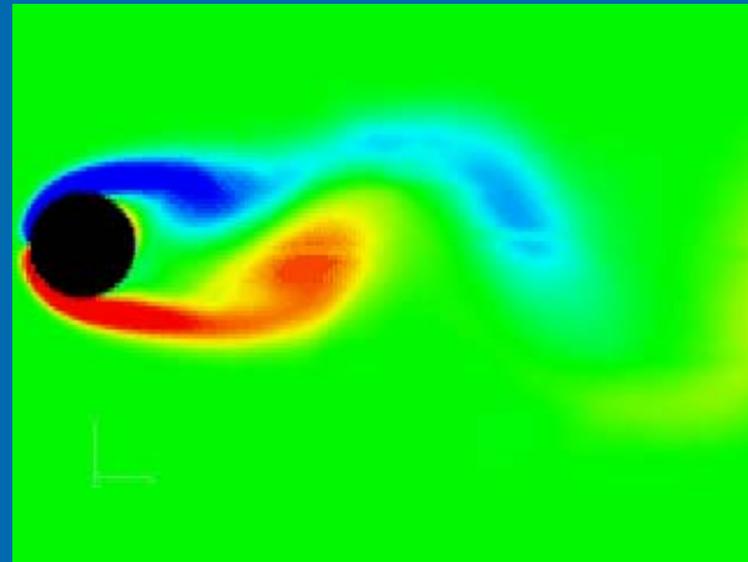


Forced flow is characterized by two different regimes:

- non lock-in: Flow (structure + temporal behavior) is independent of f_n and f_a (natural, applied freq.)
- lock-in: Flow is dependent of relationship between f_a and f_n . Lock in depends on f_a/f_n and amplitude of forcing

Sources: Gillies, 1995/97; Blevins, 1990; Williamson 1996

- The formation length gives an indication of the drag (def.: length from reference point till maximum velocity fluctuation)



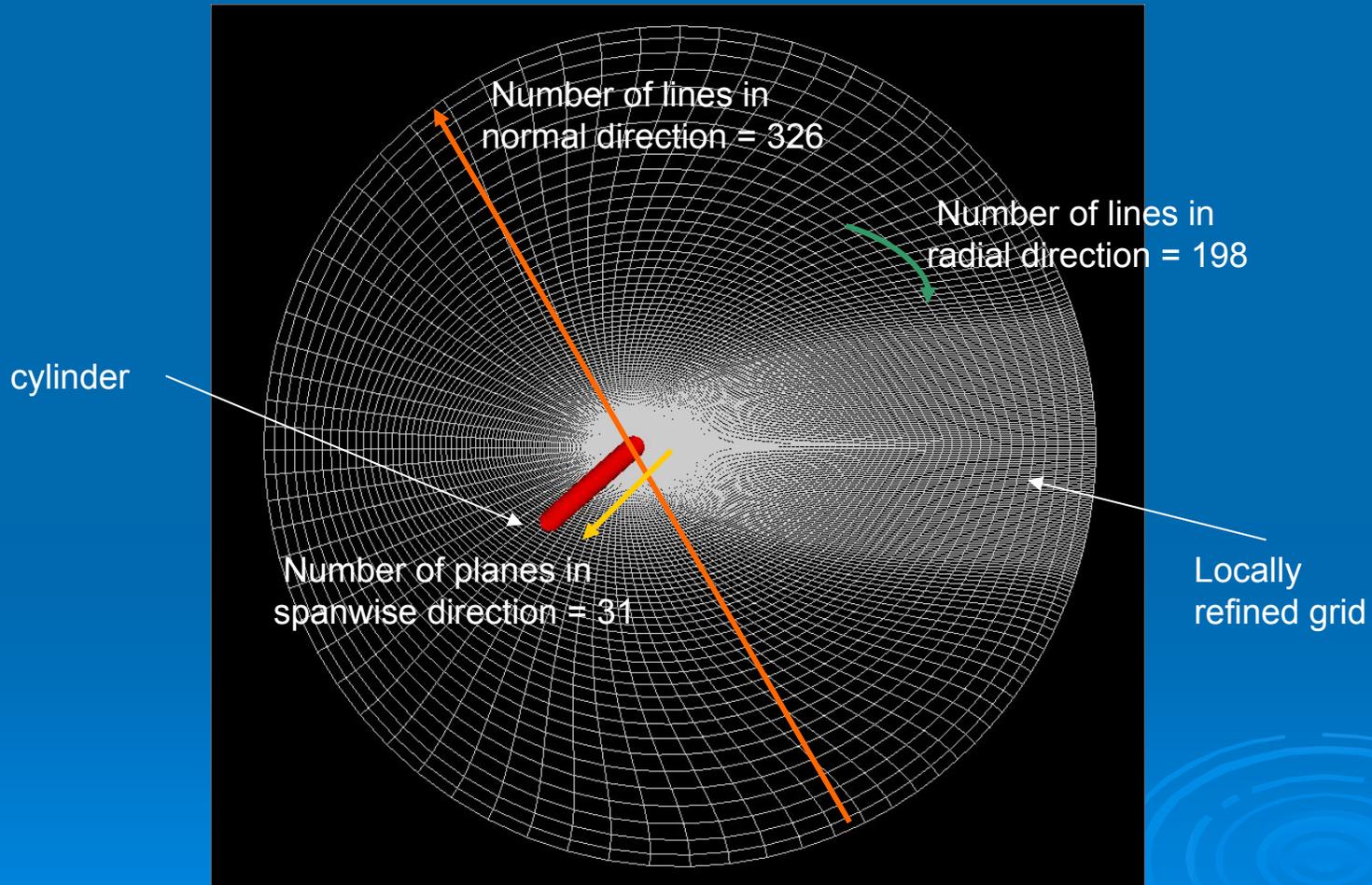


- Cobalt as flow solver
 - Finite Volume, cell-centered, 2nd order spatial and temporal (5 Newton subiter.)
- Structured grid (number of Nodes=990388; 952560 cells)
- Computational domain
 - $-17d < x < 21d$; $-19d < y < 19d$; $0 < z < 96d$
- Computational time step: $\Delta t U_{\infty} / d = 0.05$
- About 130 time steps per shedding cycle

CFD Computations



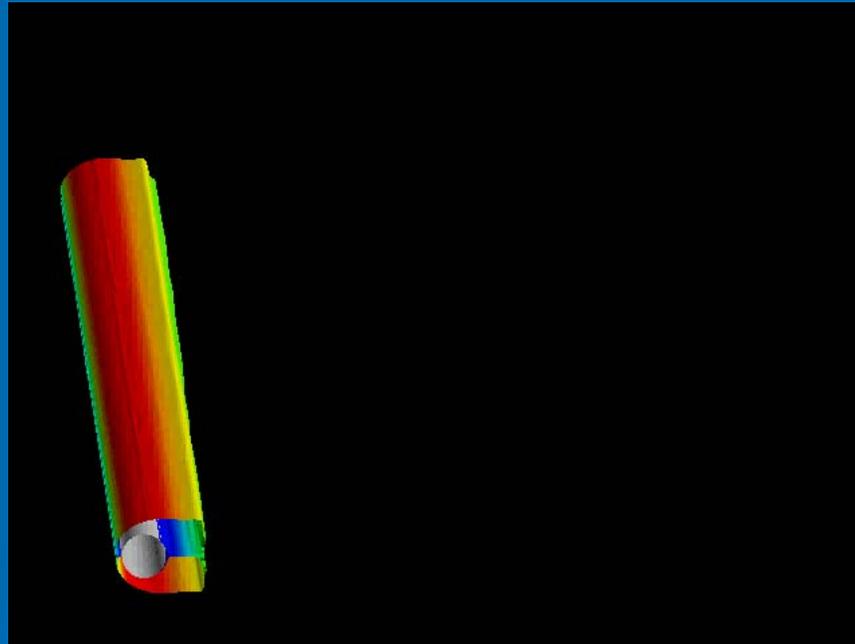
Computational grid (3D)



!But first a cool movie!



Isoplanes of Z-vorticity colored by U-Velocity

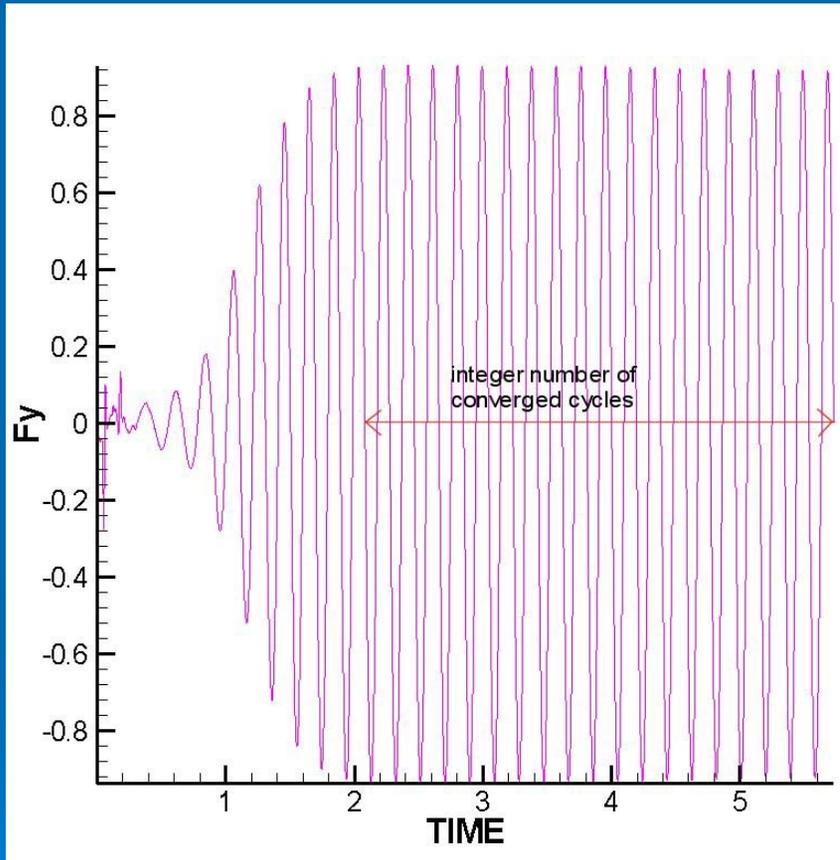


Unforced flow field, $Re=100$

CFD Computations (cont)

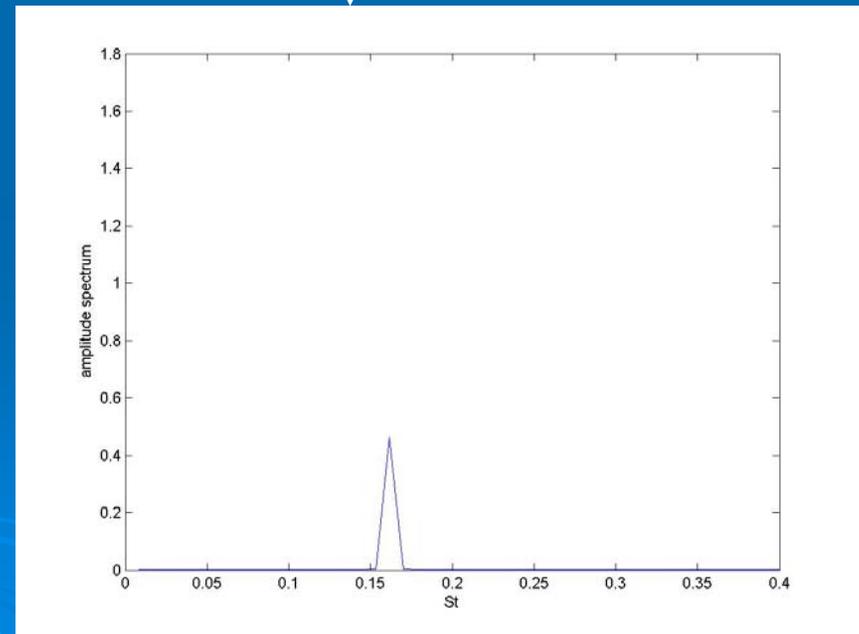


Method for determining the Strouhal number



This method is not accurate to this specific case

FFT analysis





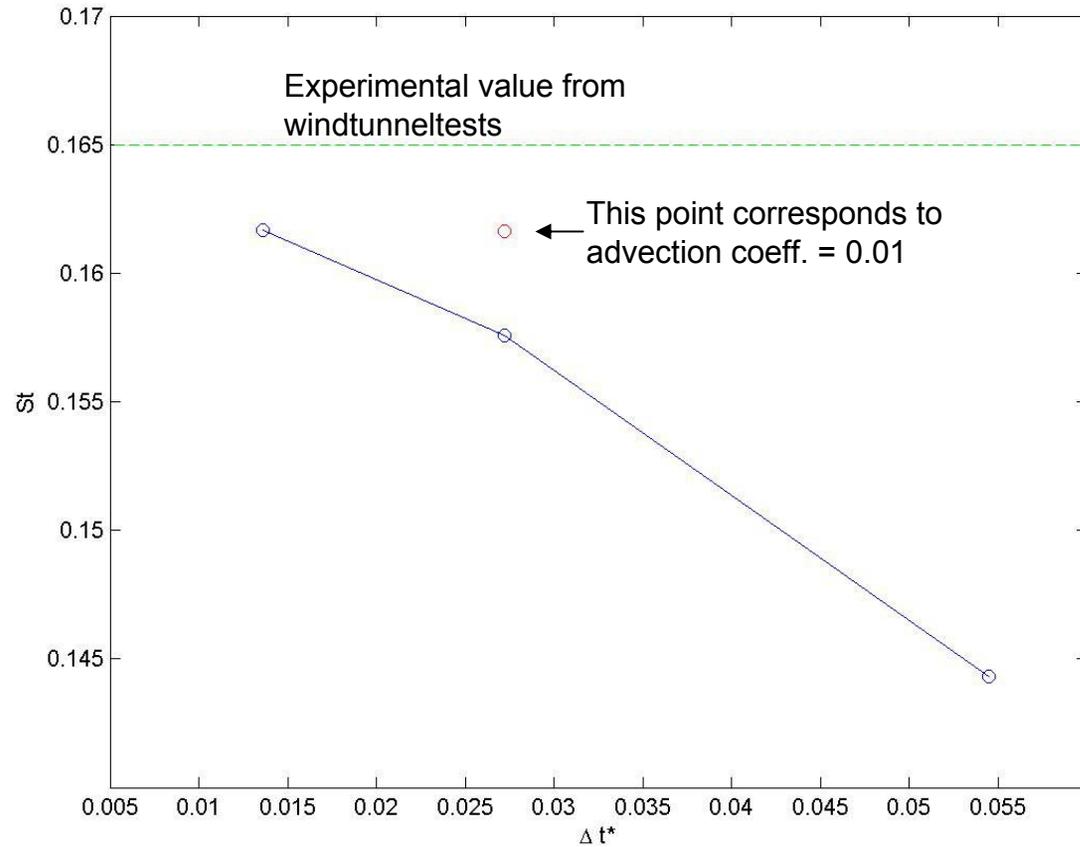
Method for determining the
Strouhal number (cont)

- FFT is not accurate here because it is very sensitive to small changes in the amount of data
- A simple approach works better: Count number of cycles based on the peaks of the normal force and divide by time to estimate the shedding freq.

CFD computations



Time step study ! 2D !



Advection coeff. = 0.02

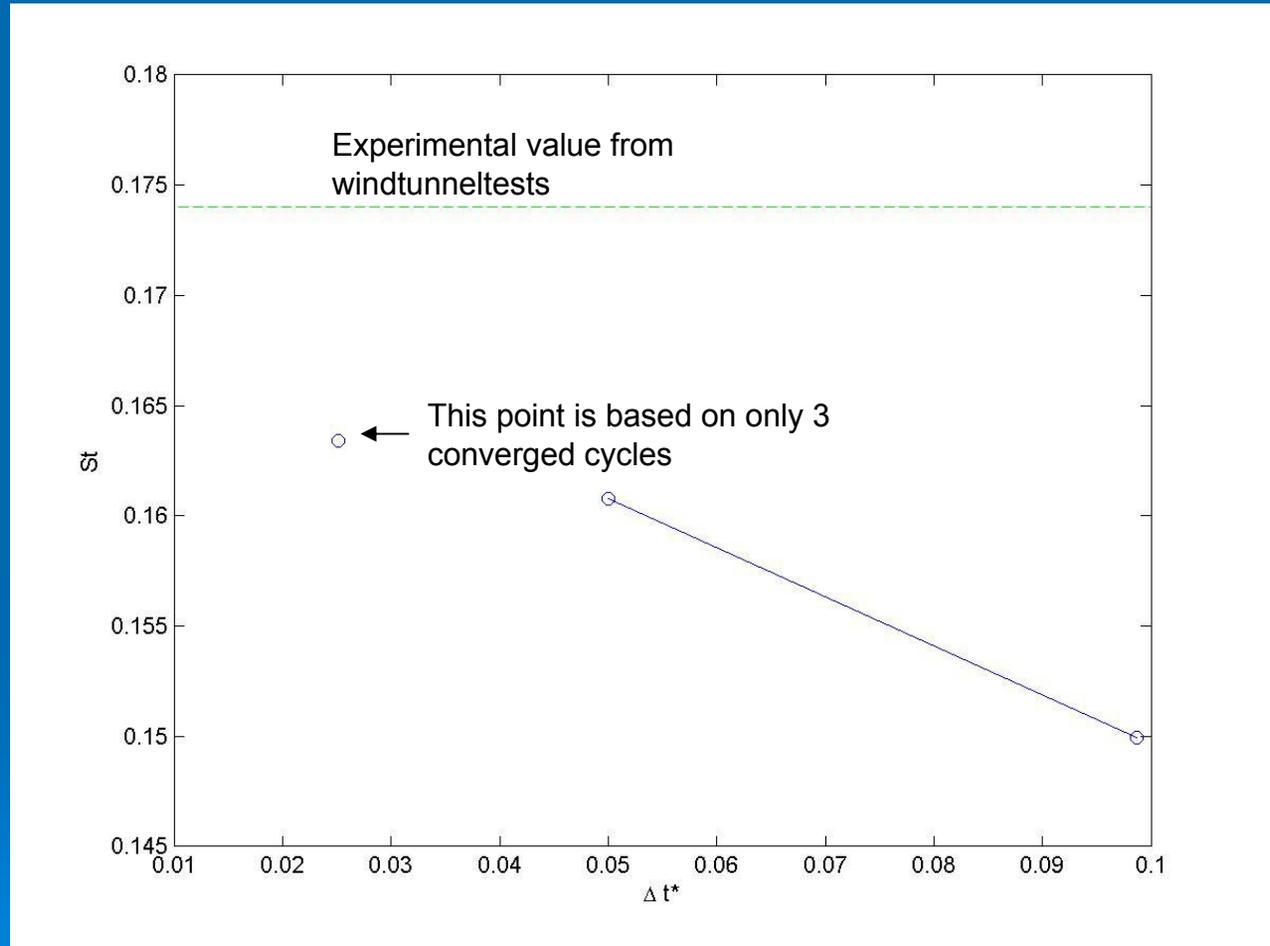
Diffusion coeff. = 0.01

M=0.1; Re=100

CFD Computations (cont)



Time step study 3D



Advection coeff. = 0.02

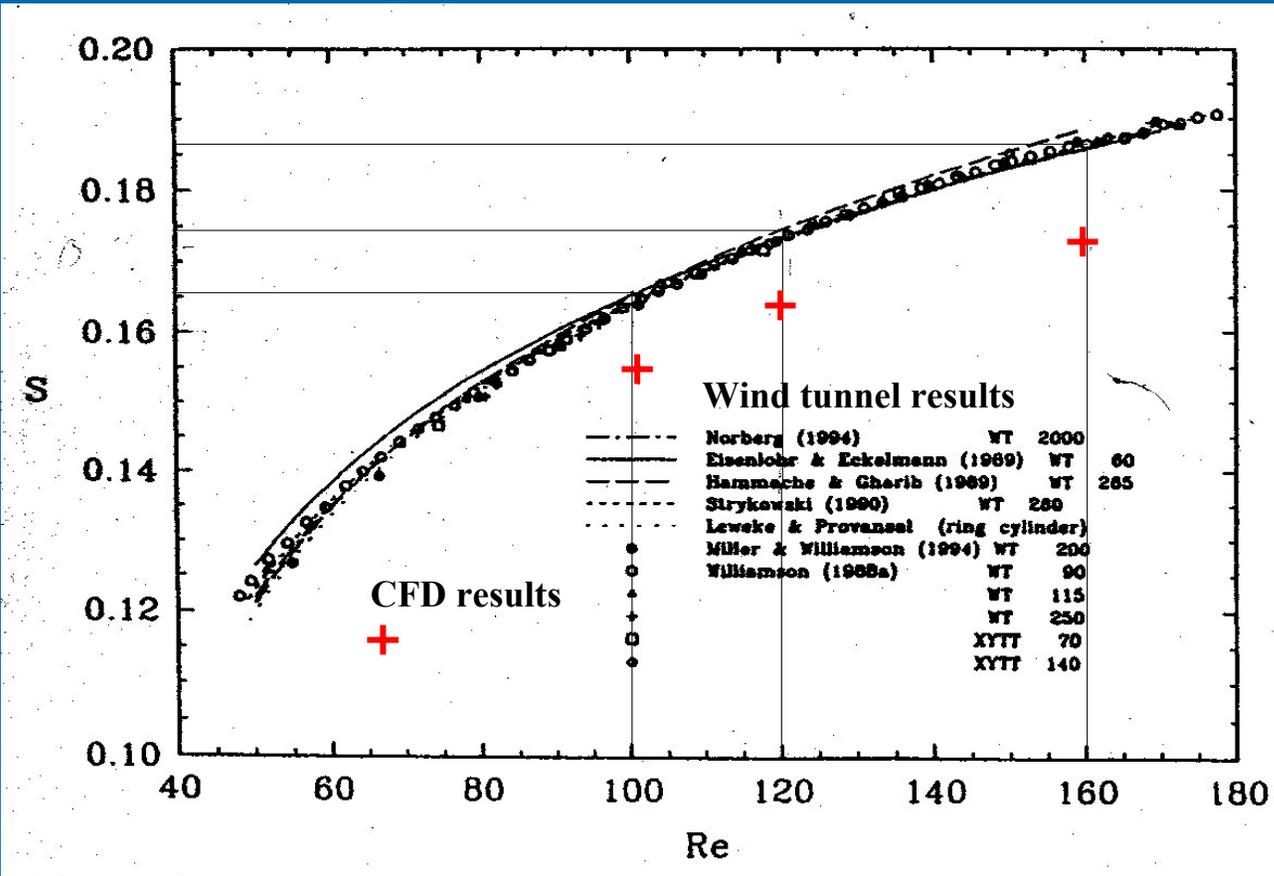
Diffusion coeff. = 0.01

M=0.1; Re=120

CFD Computations (cont)



Comparison with experiments (3D)



Results obtained by counting cycles of normal force

CFD Data

M	Re	St	Error
0.1	100	0.15	9.1 %
0.1	120	0.16	8.6 %
0.1	160	0.17	8.1 %

Williamson, 1996



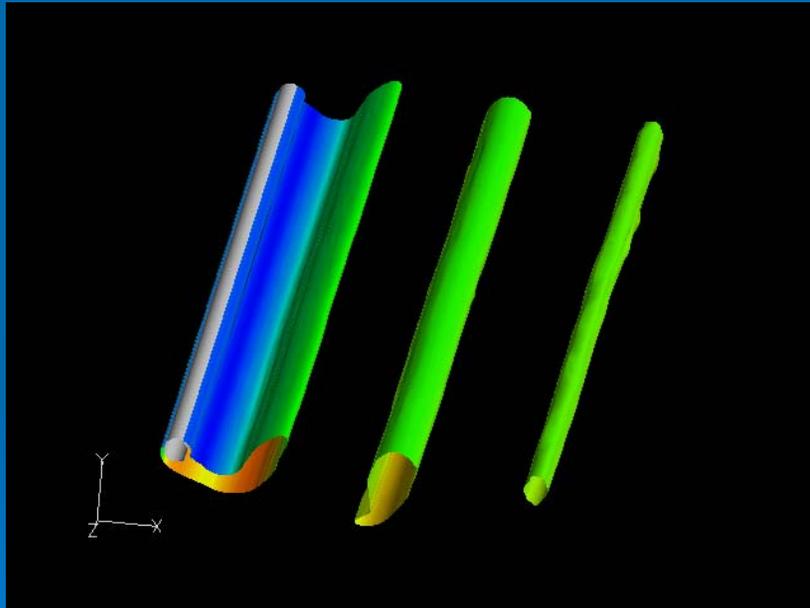
Comparison with experiments (3D), Some Remarks

- Most probably the 3D results will improve when a smaller time step is used (this can be seen from the 2D time step study)
- The cheapest solution is to adjust the advection, diffusion coefficients which can also improve the results
- The Strouhal number generally increases as the cylinder aspect ratio L/d increases (Friehe 1989)
→ maybe the resolution in spanwise direction is not sufficient

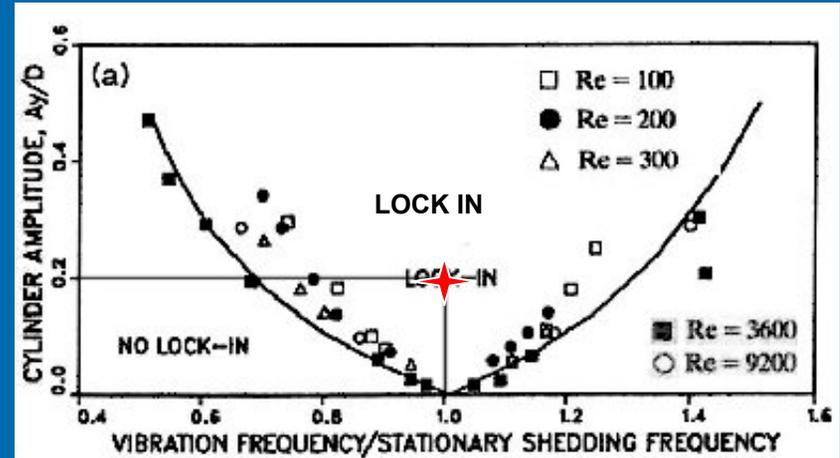
Comparison with experiments (cont)

- Phase lock in:

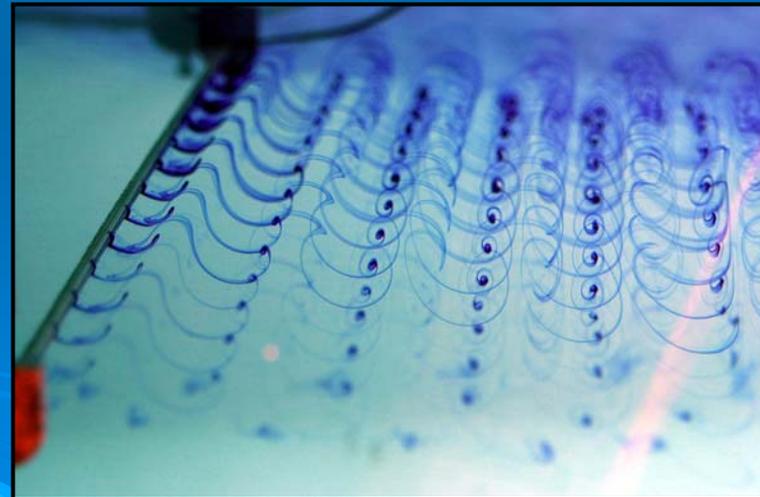
Forced cylinder motion with freq. at the vortex shedding freq. (20% amplitude)



Sinusoidal forcing
CFD Result, $Re=100$



Blevins, 1990



Water tunnel; courtesy dr. Siegel



Discussion results

- Time step study shows that the St-number converges to the right value
- Results of CFD runs are a bit lower compared to experimental data from windtunnel tests
- There is an trade off between perfect results and computation time, i.e. the model must be good enough for the control model and give results in reasonable time
- From the lock in run it can be seen that CFD captures the lock in phenomenon

Description of POD

- Experimentally, wake flows look to be dominated by a few large spatial structures → this motivates to describe the flow by its most dominant PO modes
- POD reveals coherent spatial structures within the data, the decomposition is optimal in the sense that it sorts the spatial modes with respect to their energy content
- The fluid velocity field is represented by a superposition of the empirical spatial (PO) modes multiplied by time-dependent coefficients:

$$u(x, t) \approx \sum_{k=1}^N a_k(t) \cdot \phi_k(x)$$

- It should be noted that in the present configuration only the POD modes of the U-Velocity are considered. (modes 1&2 of the U-Velocity are controlled in the present setup)

POD analysis (cont)



Description of POD (cont)



POD
(Proper
Orthogonal
Decomposition)

Mode shapes are
obtained from converged
cycles

N Temporal Mode
Amplitudes

$a_1(t)$
 $a_2(t)$
...
 $a_N(t)$

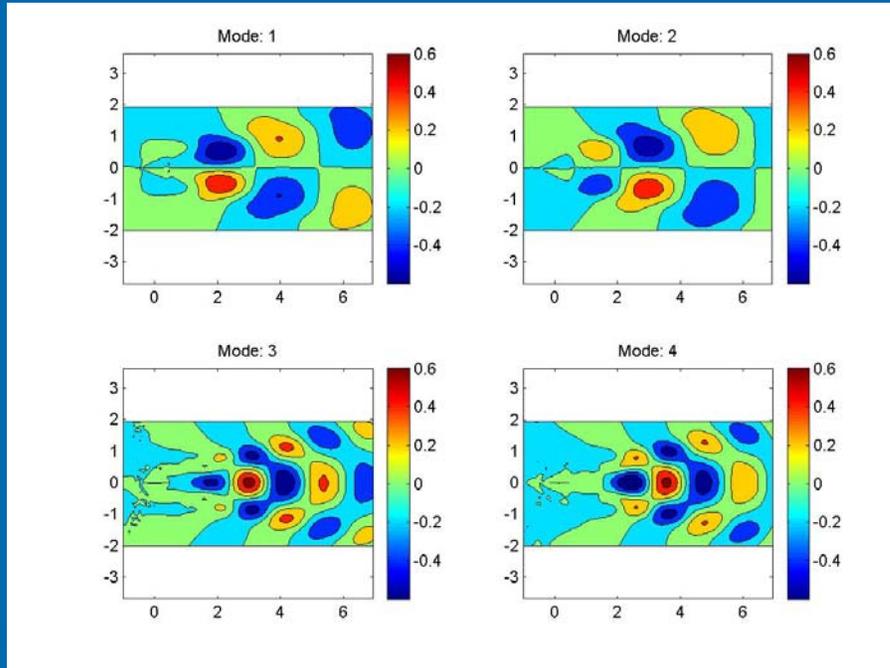
Representation of U-Velocity

$$u(x,t) \approx \sum_{k=1}^N a_k(t) \cdot \phi_k(x)$$

N Mode Shapes

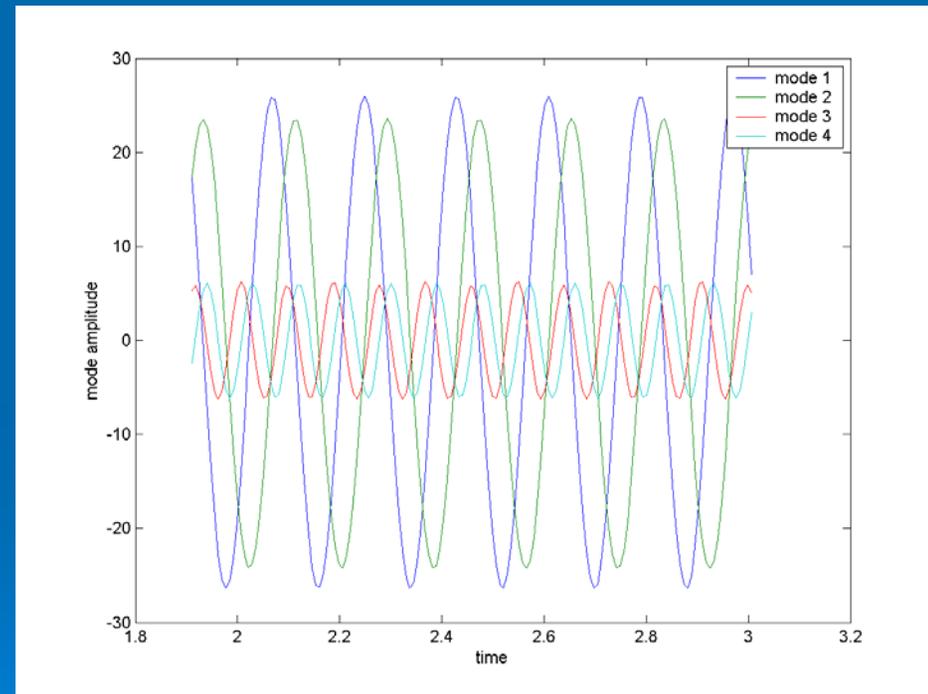
$\phi_1(x,y)$
 $\phi_2(x,y)$
...
 $\phi_N(x,y)$

2D Results



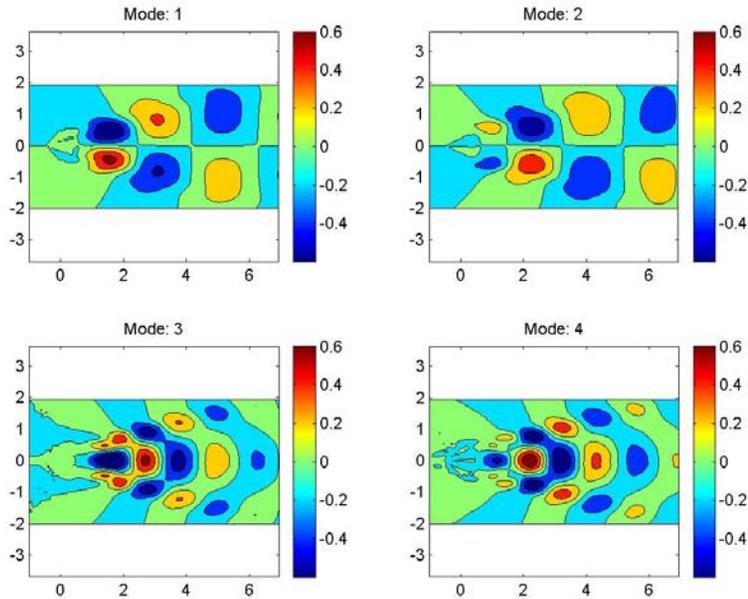
Mode Shapes

Mode Amplitudes



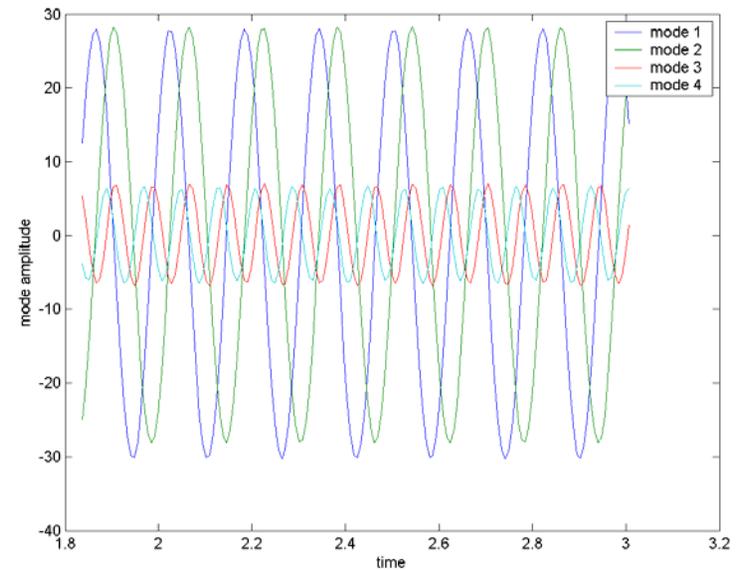
POD analysis of U-Velocity; **Re=100**

2D Results



Mode Shapes

Mode Amplitudes

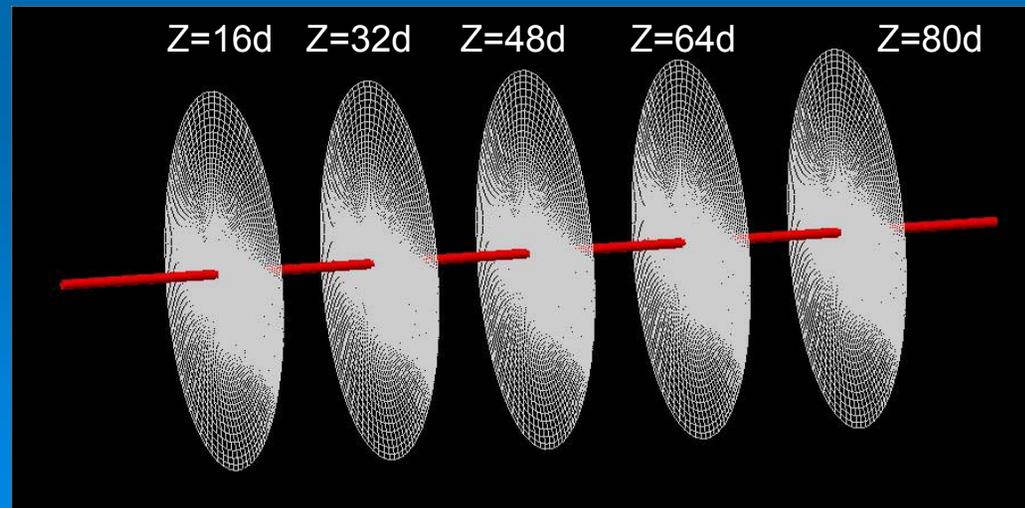


POD analysis of U-Velocity; **Re=160**

3D Results

- POD is performed on five planes in spanwise direction of the cylinder (multiples of $16d$)
- The decomposition is based upon 159 snapshots for the 2D- and, 61 snapshots for the 3D case
- By sweeping in spanwise direction the difference between the several stations can be seen

5 stations in
spanwise
direction

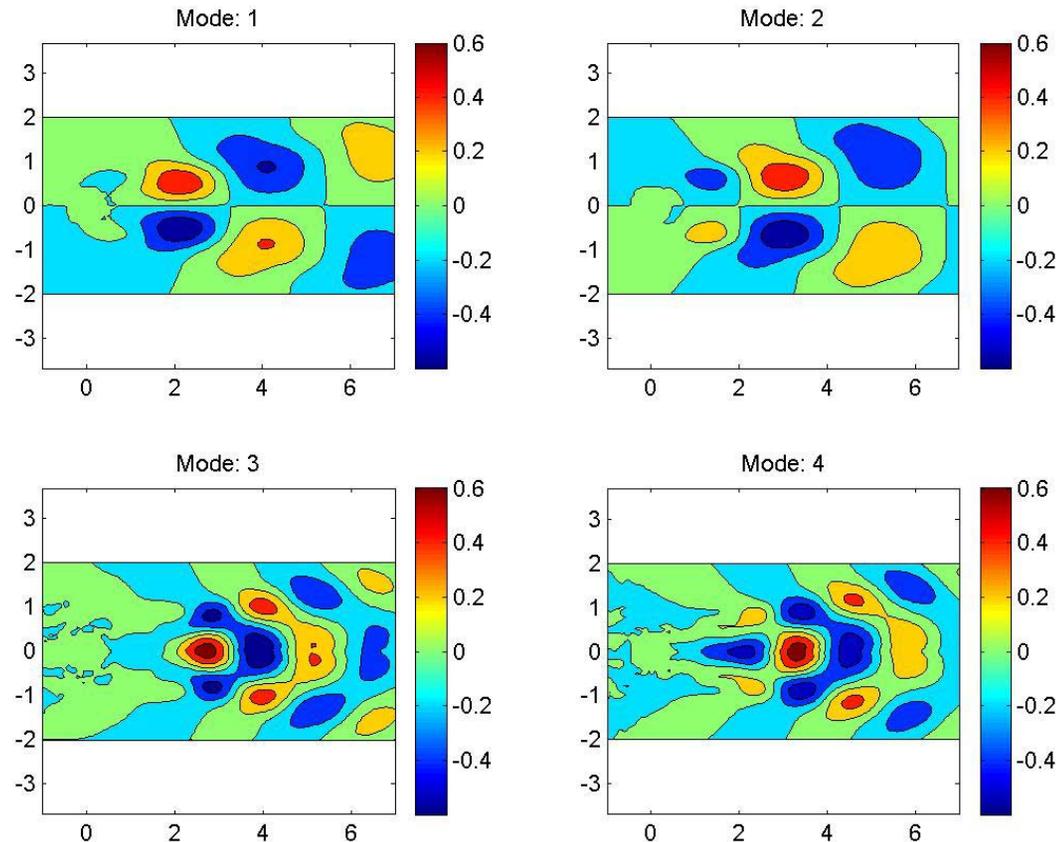


POD analysis (cont)



3D Results

station 1



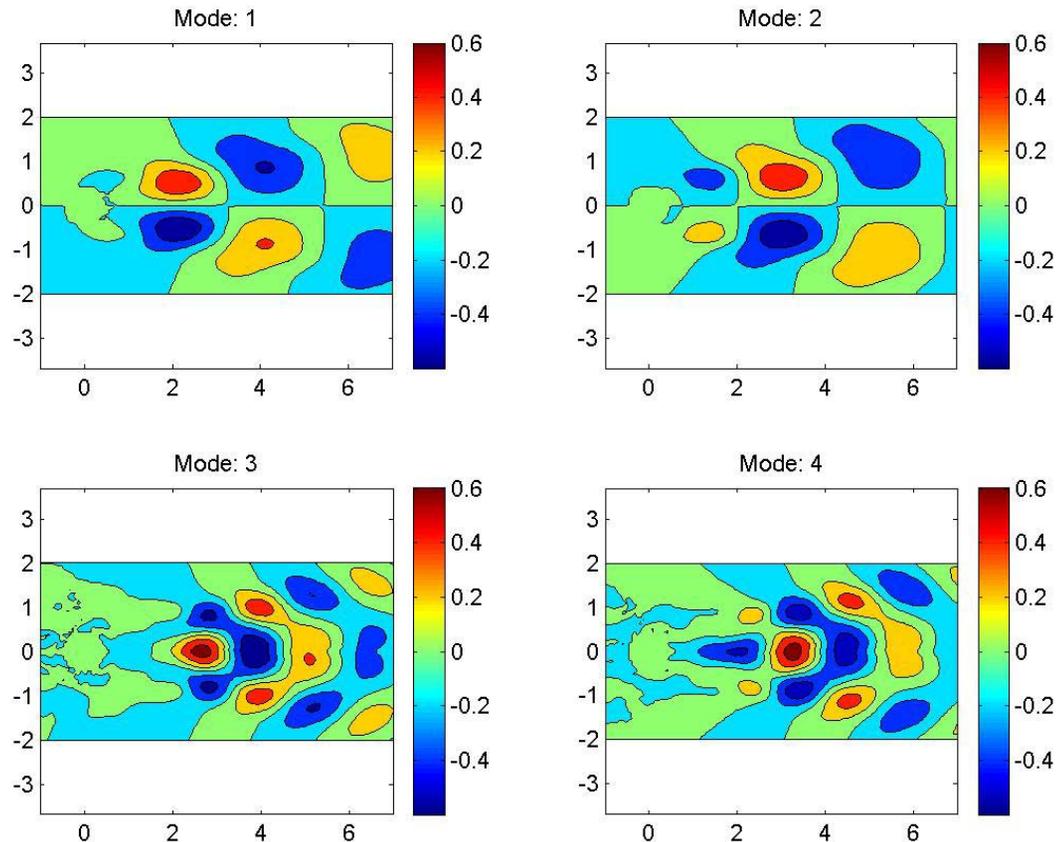
POD analysis of U-Velocity; **Re=100**

POD analysis (cont)



3D Results

station 2



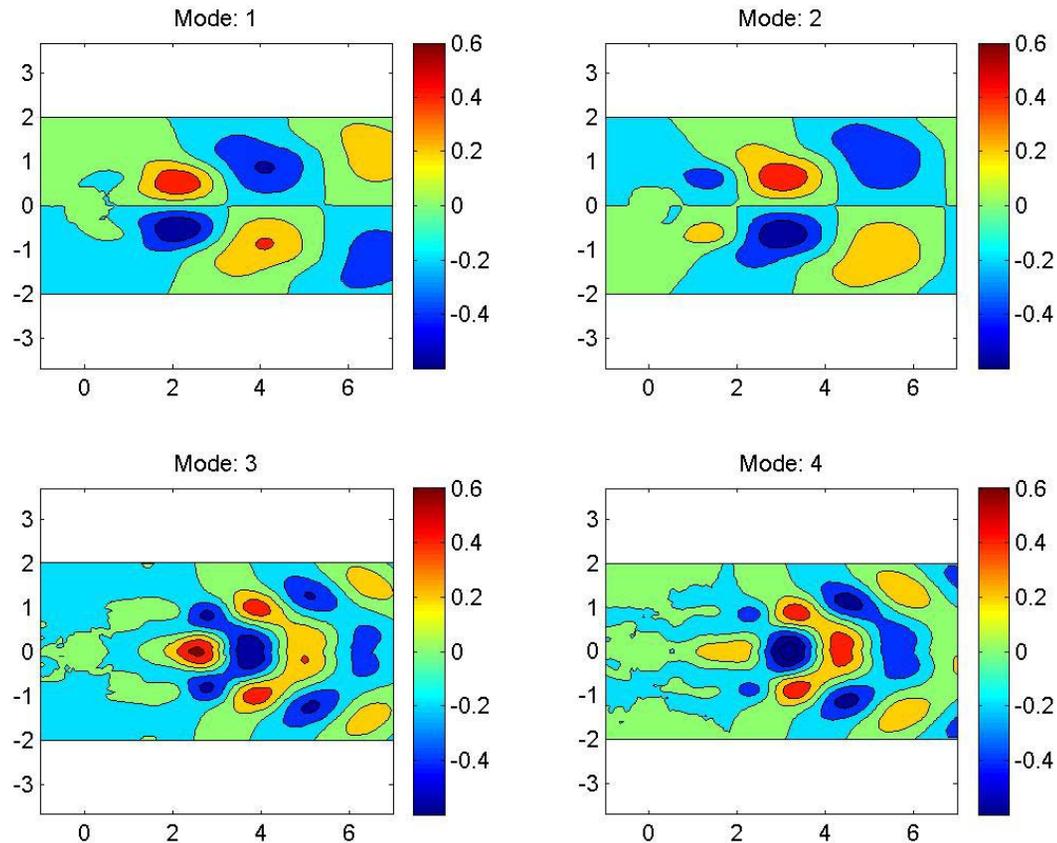
POD analysis of U-Velocity; **Re=100**

POD analysis (cont)



3D Results

station 3



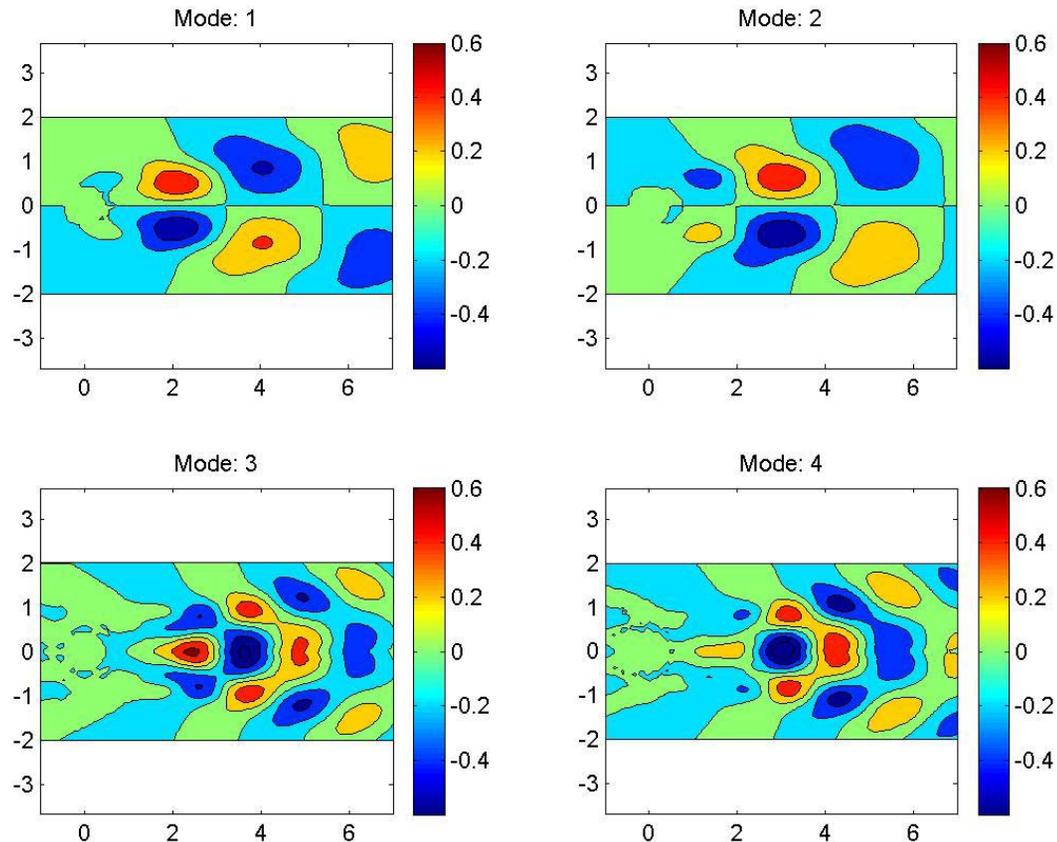
POD analysis of U-Velocity; **Re=100**

POD analysis (cont)



3D Results

station 4



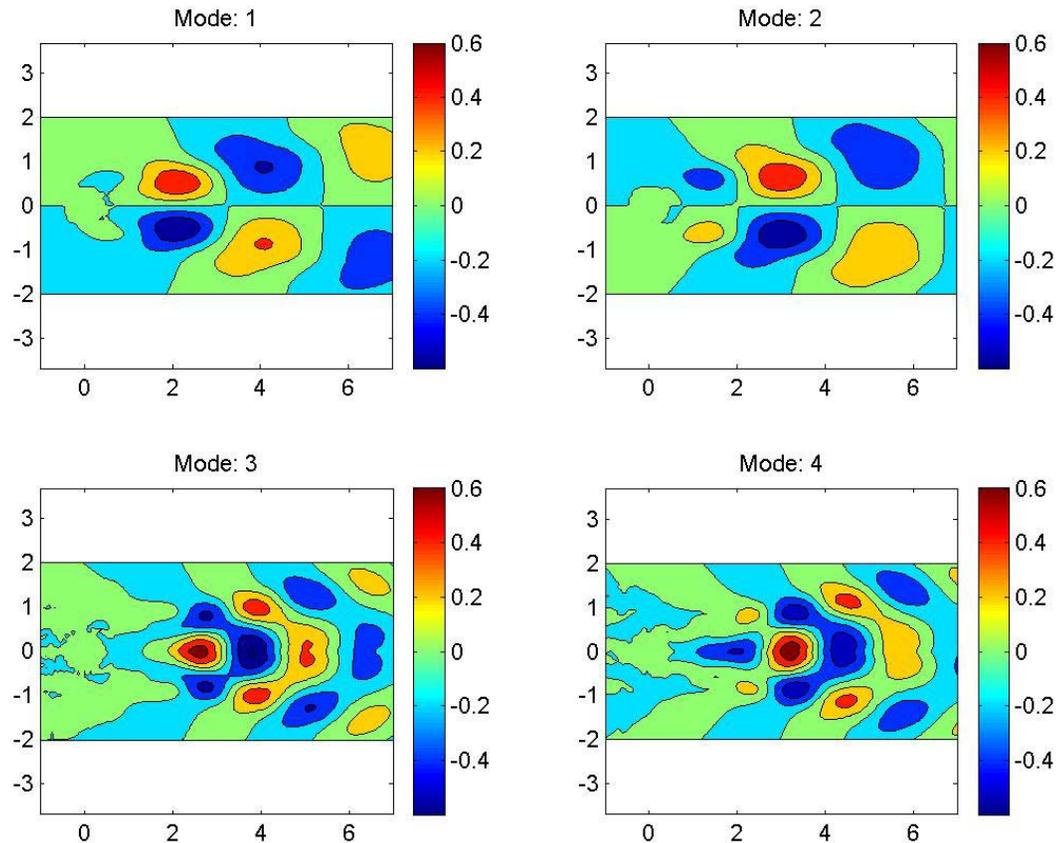
POD analysis of U-Velocity; **Re=100**

POD analysis (cont)



3D Results

station 5



POD analysis of U-Velocity; **Re=100**

- The POD modes in spanwise direction show only small differences
- Probably the differences become smaller when using more snapshots for 3D case
- From this it can be argued that the flow on the average behaves two dimensional

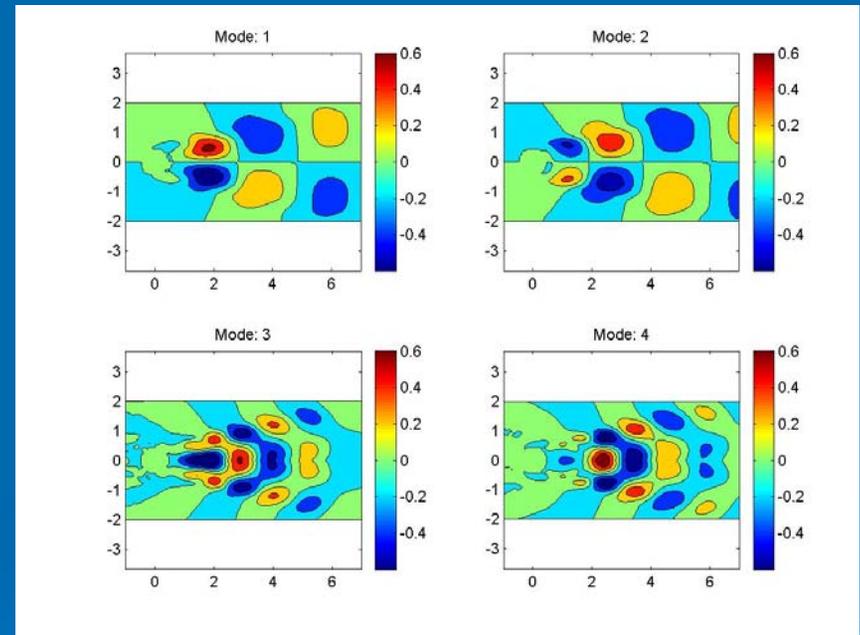
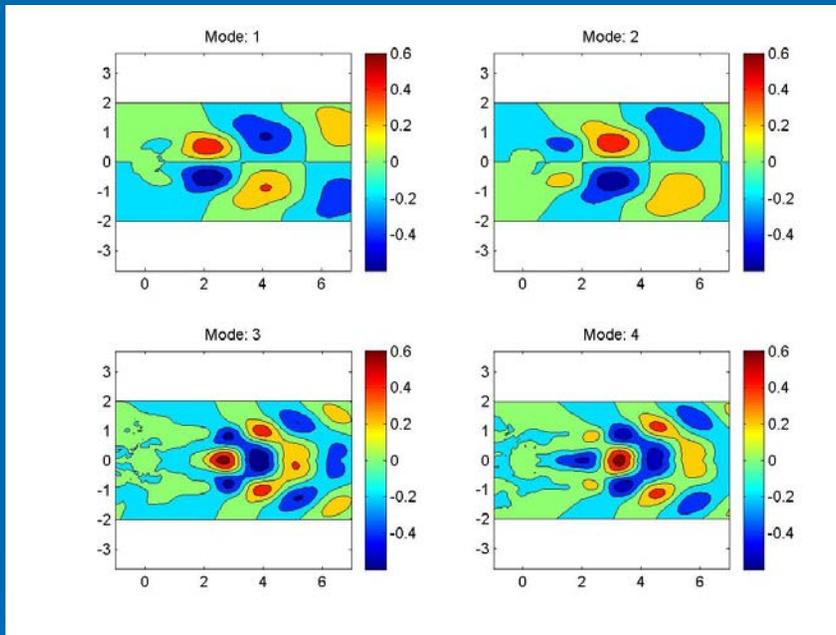
POD analysis (cont)



3D Results, comparison of $Re=100$ and $Re=160$

$Re=100, Z=32$

$Re=160, Z=32$



→ There is little difference between the two Reynolds numbers

POD analysis of U-Velocity; **$Re=100 / 160$**

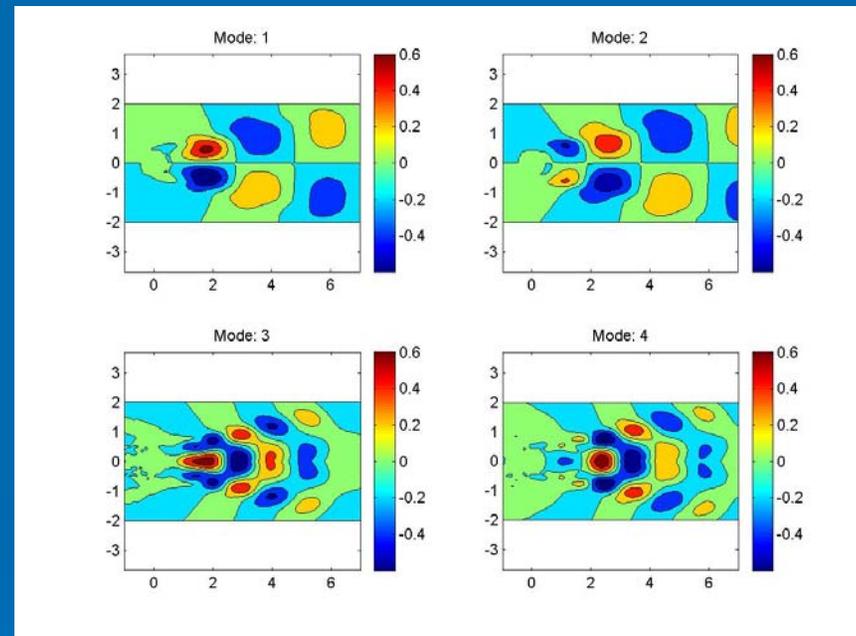
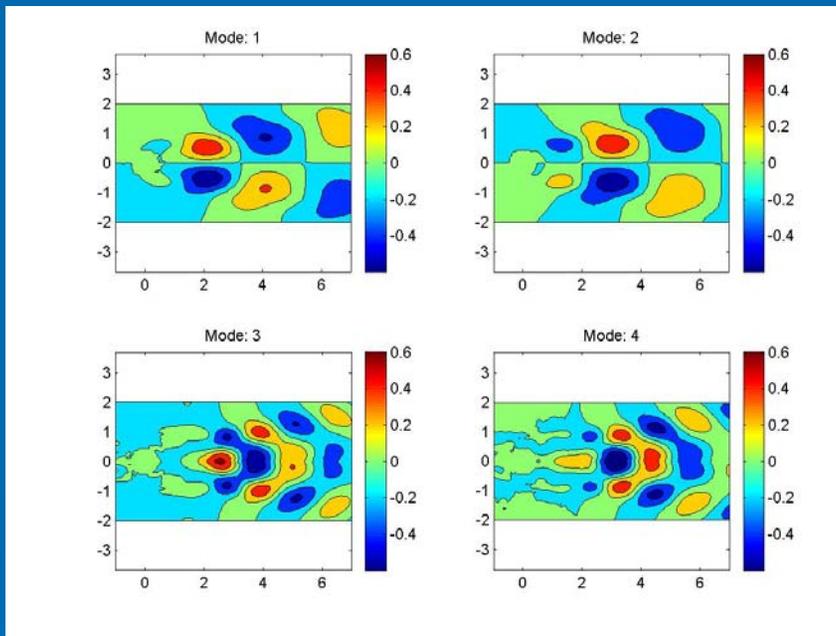
POD analysis (cont)



3D Results, comparison of $Re=100$ and $Re=160$

$Re=100, Z=48$

$Re=160, Z=48$



→ There is little difference between the two Reynolds numbers

POD analysis of U-Velocity; **$Re=100 / 160$**

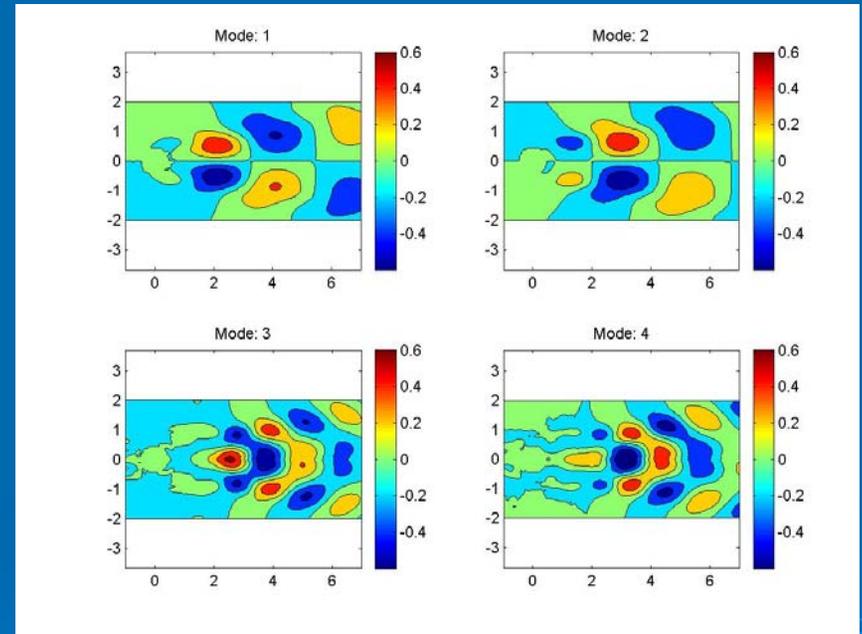
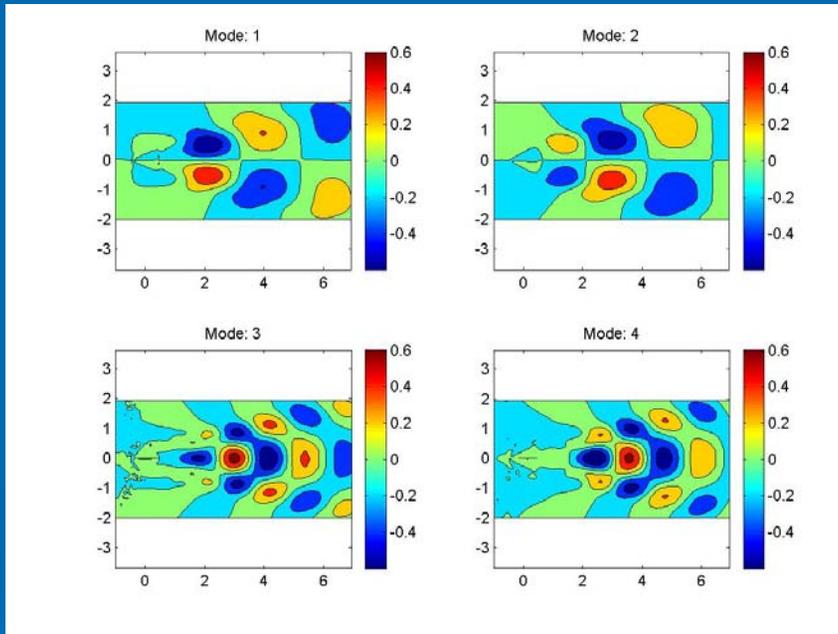
POD analysis (cont)



3D Results compared to 2D results

Re=100, 2D

Re=100, Z=48



POD analysis of U-Velocity; **Re=100**

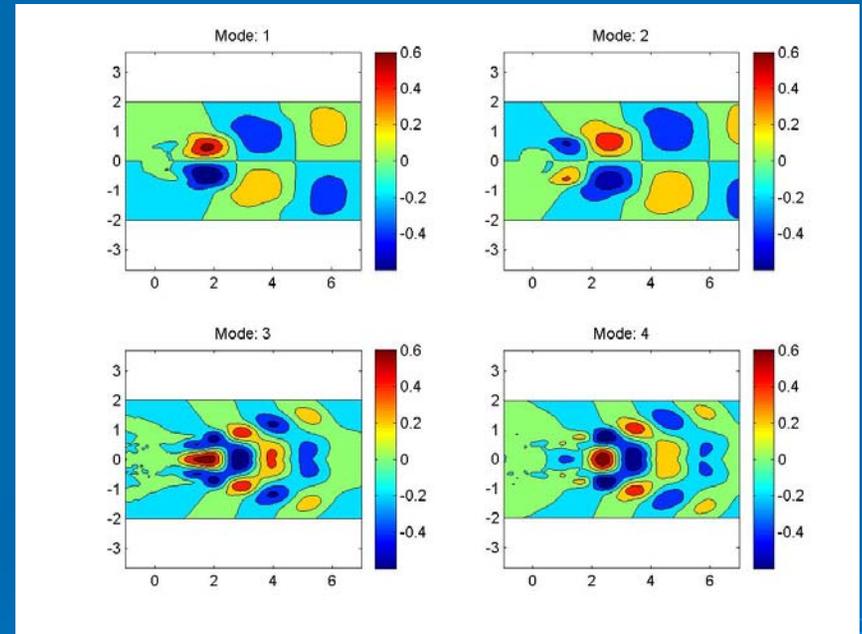
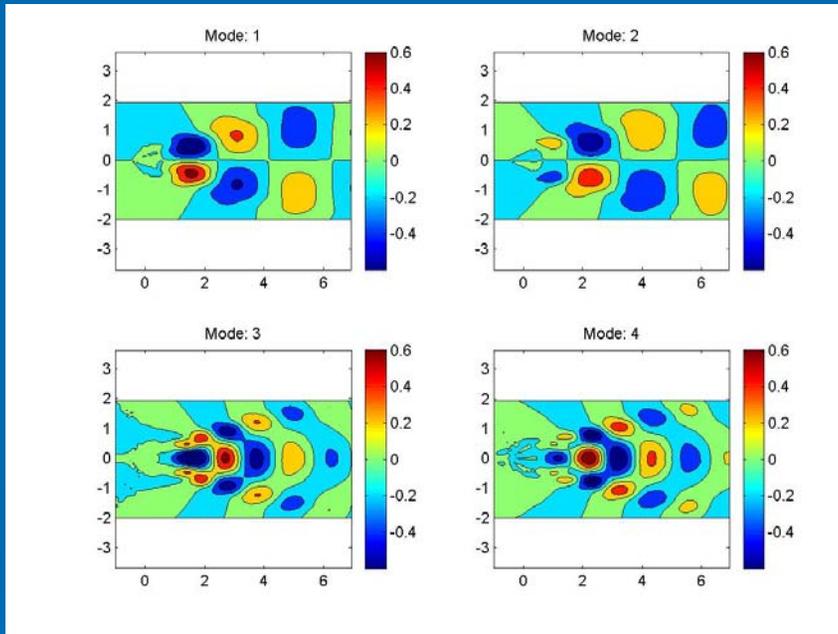
POD analysis (cont)



3D Results compared to 2D results

Re=160, 2D

Re=160, Z=48



POD analysis of U-Velocity; **Re=160**

POD analysis (cont)

3D Results compared to 2D results, Discussion



- The 3D- and 2D POD modes show similar behavior
- This is in agreement with the observations of Williamson's survey paper, who concluded from experiments that there is a 2D and 3D regime
- The first four modes contain 98% of the mean energy of the flow field → Most probable the controller will also work in three dimensions (if the controller does not excite more modes)



Future work

- A grid sensitivity study should be performed besides the time step study
- Shrink the cylinder in spanwise direction to $L/d \sim 4$ → more resolution and still a 3D flowfield (Barkley & Henderson, 1996)
- A more thorough study of POD should be performed, to come up with the best possible description of the flow field (steady-transient-controlled)
- A strong criterion for the error should be defined, to compare different POD data sets

Questions?